Electrohydrodynamics: equations and their application to paradigmatic flows

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Outline

- Electroconvection in a liquid layer subjected to unipolar injection
 - Mathematical model
 - Linear stability analysis
 - Numerical difficulties in the simulation of the electroconvection of finite amplitude

2 EHD plumes

- Assumptions
- 2D plumes
- Axisymmetric plumes
- 8 Rose-window instability
 - Introduction
 - Instability mechanism
 - Mathematical model
 - Numerical results



Mathematical model

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Mathematical model

Physical system



Figure: Geometrical configuration



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Mathematical model

Physical system



Figure: Atten and Lacroix 1978



Electroconvection in a liquid layer subjected to unipolar injection

Mathematical model



An incompressible dielectric liquid of negligible conductivity.

$$\nabla^{2} \Phi = -\frac{q}{\epsilon}$$
$$\frac{\partial q}{\partial t} + \nabla \cdot \mathbf{j} = 0$$
$$\nabla \cdot \mathbf{u} = 0$$
$$\rho \left(\frac{\partial \mathbf{u}}{\partial t} + \mathbf{u} \cdot \nabla \mathbf{u} + \nabla \rho\right) = \eta \nabla^{2} \mathbf{u} + q \mathbf{E}$$

where $\mathbf{j} = q(K\mathbf{E} + \mathbf{u} - D\nabla q)$ and $\mathbf{E} = -\nabla \Phi$.



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Electroconvection in a liquid layer subjected to unipolar injection

Mathematical model

Boundary conditions

The electric boundary conditions are:

$$\Phi(z = 0) = V$$

 $\Phi(z = d) = 0$
 $q(z = 0) = q_0$

The mechanical boundary conditions are

$$u = 0$$
 at $z = 0, d$



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Mathematical model

Non-dimensional equations

$$\nabla^{2} \Phi = -q$$

$$\frac{\partial q}{\partial t} + \nabla \cdot (q(\mathbf{E} + u) - \alpha \nabla q) = 0$$

$$\nabla \cdot \mathbf{u} = 0$$

$$\frac{T}{M^{2}} \left(\frac{\partial \mathbf{u}}{\partial t} + \mathbf{u} \cdot \nabla \mathbf{u} + \nabla p \right) = \nabla^{2} \mathbf{u} + Tq\mathbf{E}$$

with the boundary conditions:

$$\Phi(z = 0) = 1$$

 $\Phi(z = d) = 0$
 $q(z = 0) = C$
 $u = 0$ at $z = 0, d$



Mathematical model

Non-dimensional parameters

•
$$T = \frac{\epsilon V}{k\eta}$$
.

- $M = \sqrt{\epsilon/\rho}/K$. The quantity $\sqrt{\epsilon/\rho}$ is known as the Electrohydrodynamic mobility.
- $C = q_0 d^2 / \epsilon V$. Recall that $\epsilon V / d^2$ existing on the electrodes as a consequence of the applied voltage.
- $\alpha = D/KV$. Einstein's relation implies $D/K = k_B \Theta/e \sim 0.025$ V at room temperature. Therefore, $\alpha = 0.025/V$.



Mathematical model

Charge and field distribution in the hydrostatic state

$$E_{0z} = \sqrt{2j(z+b)}$$
$$q_0 = \sqrt{\frac{j}{2(z+b)}}$$

The electric boundary conditions give:

$$\sqrt{j}((1+b)^{3/2}-b^{3/2}) = rac{3}{2\sqrt{2}}$$

 $2bC^2 = j$

Theses two equations provide the current density for every value of *C*.



Electroconvection in a liquid layer subjected to unipolar injection

Mathematical model

The current density is a function of the injection level



Figure: Current density as a function of injection level.



Mathematical model

Weak and strong injection limits

• $C \to \infty$

$$E_{0z} = \frac{3}{2}\sqrt{z}$$
$$q_0 = \frac{3}{4\sqrt{z}}$$
$$j = \frac{9}{8}$$

• *C* << 1

$$E_{0z} = 1 - \frac{C}{2} + Cz + O(C^2)$$

$$q_0 = C - C^2 z + O(C^3)$$

$$j = C + O(C^2)$$

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Linear stability analysis

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Electroconvection in a liquid layer subjected to unipolar injection

Linear stability analysis

Perturbation of the hydrostatic state

$$\Phi = \Phi_0 + \delta \phi$$

$$q = Q_0 + \delta q$$

$$p = p_0 + \delta p$$

$$\mathbf{u}$$

Neglecting non-linear terms yields:

$$\nabla^{2}\delta\phi = -\delta q$$

$$\frac{\partial\delta q}{\partial t} + \nabla \cdot (\delta q \mathbf{E}_{0} + Q_{0}\delta \mathbf{E} + Q_{0}\mathbf{u}) = 0$$

$$\nabla \cdot \mathbf{u} = 0$$

$$\frac{T}{M^{2}} \left(\frac{\partial \mathbf{u}}{\partial t} + \nabla\delta p\right) = \nabla^{2}\mathbf{u} + T(Q_{0}\delta \mathbf{E} + \delta q \mathbf{E}_{0})$$

Linear stability analysis

Perturbation of the hydrostatic state

Eliminating the pressure term by taking twice the curl of equation (33). Only the z-component of the velocity is needed, which is:

$$\frac{T}{M^2}\frac{\partial \nabla^2 u_z}{\partial t} = \nabla^4 u_z + T \nabla_s^2 (\frac{d\Phi_0}{dz} \nabla^2 \delta \phi - \frac{d^3 \Phi_0}{dz^3} \delta \phi)$$



Linear stability analysis

Normal modes

Introducing normal modes:

$$u_z = u(z)e^{i(k_x x + k_y y)}e^{st}$$

$$\delta \phi = g(z)e^{i(k_x x + k_y y)}e^{st}$$

the equations become:

$$\frac{T}{M^2}s(\frac{d^2u}{dz^2}-k^2u)=(\frac{d^2}{dz^2}-k^2)^2u-k^2T(\frac{dQ_0}{dz}g-E_0(\frac{d^2}{dz^2}-k^2)g)$$

$$-s(\frac{d^{2}g}{dz^{2}} - k^{2}g) - \frac{dQ_{o}}{dz}\frac{dg}{dz} - 2Q_{0}(\frac{d^{2}g}{dz^{2}} - k^{2}g) - E_{0}\frac{d}{dz}(\frac{d^{2}g}{dz^{2}} - k^{2}g) + \frac{dQ_{0}}{dz}u = 0$$



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Linear stability analysis

Boundary conditions

The boundary conditions are expressed in terms of u and g in the following way:

$$u(0) = 0$$

$$\frac{du}{dz}(0) = 0$$

$$u(1) = 0$$

$$\frac{du}{dz}(1) = 0$$

$$g(0) = 0$$

$$g(1) = 1$$

$$\frac{d^2g}{dz^2}(0) = 0$$



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Linear stability analysis

Analytical approximative solution for weak injection

The equations simplify for C << 1 and (s = 0). With $E_0 = 1$ and $Q_0 = C - C^2 z$.

$$(\frac{d^2}{dz^2} - k^2)^2 u = k^2 T \delta \overline{q}$$
$$\frac{d}{dz} \delta \overline{q} - C^2 u = 0$$

where
$$\delta \overline{q} = -(d^2g/dz^2 - k^2g).$$

The second equation reveals the instability mechanism.



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Electroconvection in a liquid layer subjected to unipolar injection

Linear stability analysis

Galerkin method

Propose a function:

$$u(z)=z^2(1-z)^2$$

that fulfills the boundary conditions for *u*. The second equation gives:

$$\delta \overline{q} = C^2 (\frac{z^3}{3} - \frac{z^4}{2} + \frac{z^5}{5})$$

Multiplying the first equation by u and integrating between 0 and 1:

$$\int_0^1 u(\frac{d^2}{dz^2} - k^2)^2 u \, dz = k^2 T \int_0^1 u \delta \overline{q} \, dz$$



Linear stability analysis

Galerkin method

For
$$u(z) = z^2(1-z)^2$$
 this equation becomes:

$$TC^2 = \frac{20}{7}k^2 + \frac{120}{7} + \frac{1440}{k^2}$$

This function has a minimum at k = 4.74 for which $TC^2 = 197$. The exact values, determined by numerical methods, are k = 4.57 and $TC^2 = 221$.



Linear stability analysis

Numerical solution

We have a seventh order set of homogenous ordinary linear differential equations with non-constant coefficients. This problem was solved by Atten and Moreau by advanced mathematical methods.

Nowadays it can be efficiently solved by numerical algorithms commercially available. I have used the function bvp4c, available through version 6.1 of Matlab



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Linear stability analysis

The resolution provides T as a function of k



Figure: T as a function of k.



(a)

Linear stability analysis

For every value of C there is a minimum value of T



Figure: Linear stability threshold T_c as a function of injection level C.

For strong injection the instability appears at given voltage.



Numerical difficulties

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Numerical difficulties

The charge conservation equation is a first order hyperbolic equation

$$rac{\partial oldsymbol{q}}{\partial t} +
abla \cdot (oldsymbol{q}(oldsymbol{E}+u)) = oldsymbol{0}$$

Taking into account that $\nabla \cdot \mathbf{E} = q$ and $\nabla \cdot \mathbf{u} = 0$ it can be written:

$$\frac{\partial q}{\partial t} + (\mathbf{E} + u) \cdot \nabla q = -q^2$$

This is a first order partial differential equation.



Numerical difficulties

It is equivalent to the set of ordinary differential equations:

$$\frac{dq}{dt} = -q^2$$
$$\frac{dx}{dt} = u_x + E_x$$
$$\frac{dz}{dt} = u_z + E_z$$

The solution of the first equation is

$$q(t)=\frac{q_0}{1+q_0t}$$

The value of q at a given point is determined by the characteristic line connecting that point to the boundary.



Numerical difficulties

Numerical diffusion

The origin of numerical diffusion can be understood from a simplify analysis. Consider the one dimensional equation:

$$\frac{\partial q}{\partial t} + \frac{\partial uq}{\partial x} = 0$$

Assuming *u* constant and u > 0, typical finite-difference *upwind* discretization of this equation in a mesh $\{x_i\}_{i=1, Idots, m}$ is:

$$q_i^{t+\Delta t} = q_i^t - \frac{u\delta t}{\delta x}(q_i^t - q_{i-1}^t)$$

A power expansion gives:

$$q_{i}^{t+\Delta t} = q_{i}^{t} + \frac{\partial q_{i}}{\partial t} \Delta t + \frac{1}{2} \frac{\partial^{2} q_{i}}{\partial t^{2}} (\Delta t)^{2} + O(\Delta^{3} t)$$

$$q_{i-1}^{t} = q_{i}^{t} - \frac{\partial q_{i}}{\partial x} \Delta x + \frac{1}{2} \frac{\partial^{2} q_{i}}{\partial x^{2}} (\Delta x)^{2} + O(\Delta^{3} x)$$



Numerical difficulties

Taking $\partial/\partial t$ in the original equation, with *u* constant, is

$$\frac{\partial^2 q}{\partial t^2} + u \frac{\partial^2 q}{\partial x \partial t} = 0$$

Collecting the terms we get:

$$\frac{\partial q}{\partial t} + \frac{\partial uq}{\partial x} = \alpha_N \frac{\partial^2 q}{\partial x^2} + O(\Delta^2 t, \Delta^2 x)$$

with

$$\alpha_N = \frac{1}{2}u\Delta x(1-\frac{u\Delta t}{\Delta x})$$

The numerical errors behave diffusively. For $\Delta x \sim 1/100$, $u \sim 1$ and $\Delta t \sim 1/200$ is $\alpha_N \sim 2.5 \times 10^{-3}$.



EHD plumes

Assumptions

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EHD plumes

Assumptions





Physical system



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EHD plumes

Assumptions





Schlieren image



EHD flows		
EHD plumes		
Assumptions		

- The electric field is consider to be constant $\mathbf{E} = E_0 \mathbf{e}_z = (V/d) \mathbf{e}_z$.
- Charge diffusion and drift are neglected (u >> KE).
- The structure of the flow is that of a boundary layer flow. In this case this implies neglecting $\partial^2 u/\partial z^2$ in front of $\partial^2 u/\partial x^2$.
- The flow is steady.
- The pressure is constant. This will not be the case if recirculation or wall effects are not negligible.



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EHD plumes

2D plumes

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EHD plumes

2D plumes



$$\frac{\partial u_x}{\partial x} + \frac{\partial u_z}{\partial z} = 0$$
$$u_x \frac{\partial u_x}{\partial x} + u_z \frac{\partial u_z}{\partial z} = \nu \frac{\partial^2 u_x}{\partial x^2} + \frac{1}{\rho} q E_z$$
$$u_x \frac{\partial q}{\partial x} + u_z \frac{\partial q}{\partial z} = 0$$



EHD plumes

2D plumes

Boundary conditions

$$u_x = rac{\partial u_z}{\partial x} = rac{\partial q}{\partial x} = 0$$
 at $x = 0$
 $u_x = q = 0$ for $x \to \infty$

The electric current through any section is invariant:

$$J=\int_{-\infty}^{\infty}qu_{z}\,dx$$

To fix J is equivalent to assign a level of injection to the injector.



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EHD plumes

2D plumes

Similarity method

Basic idea

• If they are conveniently scaled, the velocity and charge profile have the same form at every section.

Using the stream function $\Psi(x, z)$:

$$u_x = -\partial \Psi / \partial z$$
 $u_z = \partial \Psi / \partial x$

We look for a solution of the type:

$$\eta = c(z)x, \quad \Psi = \nu d(z)f(\eta), \quad q = a(z)g(\eta)$$



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EHD plumes

2D plumes

Similarity method

Chosing the constants appropriately

$$\eta = \left(\frac{JE}{16\rho\nu^3}\right)^{1/5} \frac{x}{z^{2/5}}$$

$$\Psi = 4\nu \left(\frac{JE}{16\rho\nu^3}\right)^{1/5} z^{3/5} f(\eta)$$

$$q = \left(\frac{\rho J^4}{64\nu^2 E}\right) z^{-3/5} g(\eta)$$

The underlying idea of the method is that as long as the flow is open there is not a typical length scale.



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EHD flows EHD plumes 2D plumes

The profiles of velocity and charge are given by the solution of

$$f''' + \frac{12}{5}ff'' - \frac{4}{5}f'^2 - g = 0$$

$$f'g + fg' = 0$$

along with the boundary conditions

$$egin{array}{ll} f=f'=g'=0 & ext{at} & \eta=0 \ f'=0 & ext{for} & \eta
ightarrow\infty \ \int_{-\infty}^{\infty}f'g\,d\eta & = & 1 \end{array}$$

The second equation and the boundary conditions imply that

$$g = 0$$

except at $\eta = 0$

EHD plumes

2D plumes

Singularity at the origin

The charge profile can be expressed:

$$g(\eta) = g_0 \delta(\eta)$$

Integrating between 0 and 0⁺

$$f''' + \frac{12}{5}ff'' - \frac{4}{5}f'^2 - g = 0$$

gives a new boundary condition

$$f'(0^+)f''(0^+) + \frac{1}{2} = 0$$



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EHD plumes

2D plumes

Equivalent problem

The profile of velocity is solution of

$$f''' + \frac{12}{5}ff'' - \frac{4}{5}f'^2 = 0$$

with boundary conditions

$$f'(0^+)f''(0^+) + \frac{1}{2} = 0$$

$$f(0^+) = 0$$

$$f'(\infty) = 0$$



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EHD plumes

2D plumes

Velocity profile





EHD plumes

2D plumes

Comparison with a thermal plume

For a thermal plume the second equation is

$$g''+\frac{12}{5}\mathsf{Pr}(f'g+\mathit{f}g')=0$$

whose solution is

$$g(\eta) = g(0) \exp - \left(rac{12}{5} \operatorname{Pr} \int_0^\eta f(s) \, ds
ight)$$

Conclusion

- Thermal plumes in the limit of infinite Prandtl number are similar to EHD plumes.
- The thickness of the charge region plays the role of the thickness of the thermal layer.



EHD plumes

Axisymmetric plumes

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EHD plumes

Axisymmetric plumes



$$\frac{\partial r u_z}{\partial z} + \frac{\partial r u_r}{\partial r} = 0$$

$$u_z \frac{\partial u_z}{\partial z} + u_r \frac{\partial u_r}{\partial r} = \frac{\nu}{r} \frac{\partial}{\partial r} (r \frac{\partial u_z}{\partial r}) + \frac{1}{\rho} q E_z$$

$$u_r \frac{\partial q}{\partial r} + u_z \frac{\partial q}{\partial z} = 0$$



EHD plumes

Axisymmetric plumes

Boundary conditions

$$u_r = rac{\partial u_z}{\partial r} = rac{\partial q}{\partial r} = 0$$
 at $r = 0$
 $u_z = q = 0$ for $r \to \infty$

To these conditions the constancy of the electric current on any section of the flow must be added:

$$J=2\pi\int_0^\infty q u_z r\,dr$$



EHD plumes

Axisymmetric plumes

Similarity method

Introducing the stream function Ψ :

$$u_r = -\frac{1}{r} \partial \Psi / \partial z$$
 $u_z = \frac{1}{r} \partial \Psi / \partial r$

Following a similar procedure gives

$$\eta = \left(\frac{JE}{2\pi\rho\nu^3}\right)^{1/4} \frac{r}{z^{1/2}}$$
$$\Psi = 4\nu z f(\eta)$$
$$q = \frac{J}{2\pi\nu z} g(\eta)$$

The exponents of the scaling laws are different

- $\eta \sim x/z^{2/5}$ for 2D plumes
- $\eta \sim r/z^{1/2}$ for axisymmetric plumes



The profiles of velocity and charge are given by the solution of

$$\frac{f'''}{\eta} + \frac{f-1}{\eta} \left(\frac{f'}{\eta}\right) + g = 0$$
$$f'g + fg' = 0$$

along with the boundary conditions

$$(rac{f'}{\eta})'=rac{f}{\eta}-rac{1}{2}f''=g'=0 \quad ext{at} \quad \eta=0$$
 $rac{f'}{\eta}=g=0 \quad ext{for} \quad \eta o \infty$
 $\int_0^\infty f'g\,d\eta = 1$



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EHD plumes

Axisymmetric plumes

Singularity at the origin

- A delta function does not give a finite velocity.
- In the thermal problem the velocity at the axis diverges as

$$rac{f'}{\eta}(\eta=0)\simeq \sqrt{\ln {\mathsf{Pr}}}$$

Therefore, for axisymmetric EHD plumes it is

$$rac{f'}{\eta}(\eta=0)\simeq \sqrt{\ln(-a^2)}$$

with *a* the thickness of the charged layer in η coordinates.

Conclusion

 Unlike the 2D case, the velocity at the axis of axisymmetric plumes depends on the thickness of the charged layer. However, this dependency is very weak

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Rose-window instability

Introduction

Introduction

Experimental setup V Experimental set up



Olive oil (ohmic) at 10.75 kV



Introduction



Silicone oil (non ohmic) at 5 kV



Silicone oil (non ohmic) at 6 kV

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Differences

- Ohmic regime → large convection cells (Rose-Window instability)
- Non-ohmic regime —> two different patterns coexist



Instability mechanism

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Rose-window instability

Instability mechanism

Instability mechanism for Rose-window pattern



Simplified configuration



Rose-window instability

Instability mechanism

Instability mechanism for Rose-window pattern



(ohmic behavior)



Instability mechanism

Instability mechanism for Rose-window pattern



Electric field for an unperturbed interface

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Instability mechanism

Instability mechanism for Rose-window pattern



Electric field (perturbed)

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Rose-window instability

Mathematical model

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Rose-window instability

Mathematical model

Equations in the air region

$$\nabla^2 \phi = -\frac{q}{\epsilon_0},$$

$$\frac{\partial \boldsymbol{q}}{\partial t} + \nabla \cdot \mathbf{J} = \mathbf{0}.$$

with $\mathbf{J} = qK_a\mathbf{E}$

$$-\nabla \boldsymbol{\rho} + \rho_{\boldsymbol{a}} \boldsymbol{g} \boldsymbol{e}_{\boldsymbol{z}} + \boldsymbol{q} \boldsymbol{\mathsf{E}} = \boldsymbol{\mathsf{0}},$$

Air motion is neglected



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Rose-window instability

Mathematical model

Equations for the liquid region (Ohmic regime)

$$\nabla^2 \phi = \mathbf{0},$$
$$\nabla \cdot \mathbf{J} = \mathbf{0}$$

with $\mathbf{J} = \sigma \mathbf{E}$

 $\nabla \cdot \mathbf{u} = \mathbf{0},$ $\rho_l (\frac{\partial \mathbf{u}}{\partial t} + \mathbf{u} \cdot \nabla \mathbf{u}) = -\nabla p + \rho_l g \mathbf{e}_z + \eta \nabla^2 \mathbf{u}$ no electric body force



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Mathematical model

Boundary conditions at the electrodes

$$\phi = V \quad \text{at} \quad z = -L,$$

$$q = q_0 \quad \text{at} \quad z = -L,$$

$$\phi = 0 \quad \text{at} \quad z = d,$$

$$\mathbf{u} = 0 \quad \text{at} \quad z = d.$$

charge injection



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Mathematical model

Boundary conditions at the interface (Ohmic regime)

$$[\mathbf{E}] \times \mathbf{n} = \mathbf{0}, \quad [\epsilon \mathbf{E}] \cdot \mathbf{n} = q_s.$$
$$\frac{\partial q_s}{\partial t} + \nabla_s \cdot (q_s \mathbf{u}) + [\mathbf{J}] \cdot \mathbf{n} - [q\mathbf{u}] \cdot \mathbf{n} = \mathbf{0}.$$
$$-\frac{\partial f}{\partial t} + u_z + \mathbf{u} \cdot \nabla_s f = \mathbf{0},$$



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Rose-window instability

Mathematical model

Electric stresses



Mathematical model

Equations and boundary conditions for the non-Ohmic regime

$$\frac{\partial \boldsymbol{q}}{\partial t} + \nabla \cdot \mathbf{J} = \mathbf{0},$$

where $\mathbf{J} = q(K_l \mathbf{E} + \mathbf{u})$.

$$\rho_l(\frac{\partial \mathbf{u}}{\partial t} + \mathbf{u} \cdot \nabla \mathbf{u}) = -\nabla p + \rho_l g \mathbf{e}_z + \eta \nabla^2 \mathbf{u} + q \mathbf{E}.$$

$$[\epsilon \mathbf{E}] \cdot \mathbf{n} = \mathbf{0}.$$
$$[\mathbf{J}] \cdot \mathbf{n} - [q\mathbf{u}] \cdot \mathbf{n} = \mathbf{0}.$$
$$\eta \mathbf{t} \cdot \left(\nabla \mathbf{u} + \nabla \mathbf{u}^{T}\right) \cdot \mathbf{n} = \mathbf{0}$$



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Rose-window instability

Mathematical model

Differences between both models

	Ohmic	Non-Ohmic
Electric current	$\mathbf{J} = \sigma \mathbf{E}$	$\mathbf{J} = qK_{l}\mathbf{E}$
Volume force	0	qE
Surface charge density	$[\epsilon \mathbf{E}] \cdot \mathbf{n} = q_s$	$[\epsilon \mathbf{E}] \cdot \mathbf{n} = 0$
Tangential stress at the interface	<i>q</i> ₅E ⋅ t	0



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Rose-window instability

Mathematical model

Stability study

$$\phi = \phi_{s} + \delta\phi$$

$$\delta\phi = g(z) \exp(\omega t) \exp(i(k_{x}x + k_{y}y))$$

- Ohmic case: set of 9 first order linear differential equations with 10 boundary conditions.
- Non Ohmic case: set of 10 first order linear differential equations with 11 boundary conditions.



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Numerical results

Outline

Electroconvection in a liquid layer subjected to unipolar injection

- Mathematical model
- Linear stability analysis
- Numerical difficulties in the simulation of the electroconvection of finite amplitude

2 EHD plumes

- Assumptions
- 2D plumes
- Axisymmetric plumes

8 Rose-window instability

- Introduction
- Instability mechanism
- Mathematical model
- Numerical results



Rose-window instability

Numerical results

Results



Stability diagram for an Ohmic liquid as a function of the conductivity



Numerical results



Stability parameter $U = \frac{\epsilon_0 \rho_l V^2}{\eta^2}$ as a function of the wavenumber (Ohmic case).



Numerical results



Stability parameter as a function of the wavenumber (non Ohmic case).



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Rose-window instability

Numerical results



- The mathematical equations of EHD flow are well established and tested.
- Semi-analytical methods help to understand the underlying physical mechanisms.
- The numerical resolution of EHD flows require algorithms that avoid numerical diffusion.



Rose-window instability

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